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# Electrochemical characteristics of iron carbide as an active material in alkaline batteries

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#### Abstract

Electrochemical properties of iron carbide (Fe<sub>3</sub>C) for use as an alkaline battery anode were investigated during charge–discharge cycles. Results of electrochemical measurements and Mössbauer spectroscopy suggested that Fe<sub>3</sub>C is oxidized irreversibly to Fe<sub>3</sub>O<sub>4</sub> during discharge processes and that the produced Fe<sub>3</sub>O<sub>4</sub> is subsequently changed to Fe(OH)<sub>2</sub> and Fe during the charging process, raising the discharge/charge capacity in further galvanostatic cycles. In addition, the electrode particles were observed to be less than 100 nm in diameter and to be highly dispersed on the surface of carbon black. These phenomena seems to be caused by dissolution and deposition of Fe(OH)<sub>2</sub> and Fe via intermediate iron species, leading to exposure of a fresh Fe<sub>3</sub>C surface to the electrolyte after the second discharge. © 2006 Elsevier B.V. All rights reserved.

Keywords: Alkaline battery anode; Iron carbide

#### 1. Introduction

Electrical energy is a crucially important resource for modern civilization because it is easily transportable and is readily transformable to other kinds of energy: mechanical, chemical, light or heat. However, it is difficult to store electrical energy itself. This salient obstacle prevents more efficient use of electric energy, which could be achieved by stabilizing the power output of a power plant or by power generation using renewable energy sources. Efficient and large-scale electricity storage is necessary to solve these problems. From a cost-efficiency perspective, a simple and large battery system using an inexpensive active material would be suitable. Iron has been considered as a promising active material of alkaline secondary batteries because of its low cost, large specific capacity, and long-term durability [1-6]. For this study, we chose iron carbide Fe<sub>3</sub>C, an inexpensive compound of iron, as an active material candidate. Usually, Fe<sub>3</sub>C is synthesized through the reaction of iron oxide with natural gas using a fluidized bed reactor, which makes the energy consumed in Fe<sub>3</sub>C production (15 GJ ton<sup>-1</sup> [7]) less than that consumed in pure iron production (ca.  $24 \text{ GJ ton}^{-1}$  [8]). Therefore, the appli-

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cation of Fe<sub>3</sub>C to an anode of an alkaline secondary battery instead of pure iron might save costs and energy required for producing a large-scale secondary battery, although the electrochemical characteristics of Fe<sub>3</sub>C remain largely unknown. This study investigated the characteristics of Fe<sub>3</sub>C as an active material of alkaline battery using electrochemical measurements, composition analysis and morphological observation.

## 2. Experimental

In this experiment, Fe<sub>3</sub>C particles (Kawasaki Heavy Industries, Ltd.) of 0.1–0.5-mm diameter, which were produced by reduction of iron ore using methane in a fluidized bed reactor, were used as the active material. They contain 89.5 wt.% of Fe<sub>3</sub>C and 10.5 wt.% of Fe<sub>3</sub>O<sub>4</sub>.

Particles of the active material were ground in a mortar and mixed with carbon black (Ketchen EC; Akzo Nobel Corp.) as a conductive material and polytetrafluoroethylene (PTFE) as a binder at the weight ratio of 20:4:1. After desiccation at 100 °C, the paste-like composite was applied on a 2-cm-diameter nickel foam disk, which was then pressed at 5 MPa for 5 min. Thickness of the prepared electrode was ca. 0.3 mm. A pure iron–carbon black electrode was fabricated similarly using electrolytic iron powder (Kanto Chemical Co. Inc.) of 0.1–0.2-mm

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Fig. 1. Cyclic voltammogram of Fe<sub>3</sub>C and pure iron. The potential sweep rate was  $0.5 \text{ mA s}^{-1}$ .

diameter to compare electrochemical properties with those of Fe<sub>3</sub>C.

A working electrode was soaked in the electrolyte of  $6 \text{ mol dm}^{-3}$  KOH solution for 2 h before electrochemical measurements. The electrolyte was connected electrically to a reference electrode, Ag/AgCl in saturated KCl aqueous solution, using a salt bridge of KCl. The electrolyte was kept at 25 °C during experimentation by circulating water around the electrochemical cell. Nickel wire was used as a counter electrode.

Galvanostatic potentiometry and cyclic voltammetry were carried out using a potentio/galvanostat (HZ-3000; Hokuto Denko Corp.). For galvanostatic potentiometry, the discharge and charge current density were  $50 \text{ mA g}^{-1}$ . In this measurement, the electrode was first oxidized until the potential reached -0.6 V versus Ag/AgCl in the discharge process, and then reduced until -1.2 V versus Ag/AgCl in the charge process. For cyclic voltammetry, the rest potential was -0.9 V versus Ag/AgCl and the potential scan rate was fixed at  $0.5 \text{ mV s}^{-1}$ .

To investigate the composition change of an active material in charge–discharge cycles, Mössbauer spectroscopy was performed. About 50 mg of the active material was mixed with 50 mg of boron nitride in a mortar. The mixture was pasted on a sample holder and measured using Mössbauer spectroscope (Laboratory Equipment Corp.). Composition of the sample was determined using calibration curve method. Calibration curves of Fe, Fe<sub>3</sub>O<sub>4</sub> and Fe<sub>3</sub>C were prepared using commercial products.

Morphology of Fe<sub>3</sub>C particles was observed using scanning electron microscopy (SEM).

#### 3. Results and discussion

Cyclic voltammograms of iron carbide and pure iron before the first discharge are shown in Fig. 1. In the case of pure iron, two pairs of reduction (Red)–oxidation (Ox) peaks are apparent, respectively, as Red<sub>1</sub>/Ox<sub>1</sub> and Red<sub>2</sub>/Ox<sub>2</sub> at -1.2 V/-1.0 V and -1.08 V/-0.8 V versus Ag/AgCl. These peaks are assigned, respectively, to the following reactions (1) and (2) of iron oxidation [4,5]:

$$\operatorname{Red}_1/\operatorname{Ox}_1$$
:  $\operatorname{Fe}(\operatorname{OH})_2 + 2e^- \rightleftharpoons \operatorname{Fe} + 2\operatorname{OH}^-$  (1)



Fig. 2. Cyclic voltammograms of  $Fe_3C$  in discharge–charge cycles 1–10. The potential sweep rate was  $0.5 \text{ mA s}^{-1}$ .

$$\operatorname{Red}_2/\operatorname{Ox}_2:\operatorname{Fe}_3\operatorname{O}_4 + 4\operatorname{H}_2\operatorname{O} + 2\operatorname{e}^- \rightleftharpoons 3\operatorname{Fe}(\operatorname{OH})_2 + 2\operatorname{OH}^-.$$
(2)

In the case of iron carbide, a large and broad oxidation peak  $Ox_3$  at -0.7 V versus Ag/AgCl was observed with a pair of small peaks that were similar to those of  $Ox_2/Red_2$ . Therefore, the  $Ox_3$  peak is attributable to oxidation of Fe<sub>3</sub>C. In addition, the appearance of peaks similar to  $Ox_2/Red_2$  is inferred to result from the existence of Fe<sub>3</sub>O<sub>4</sub> because Fe<sub>3</sub>C particles contain 10.5 wt.% of Fe<sub>3</sub>O<sub>4</sub>.

Fig. 2 shows cyclic voltammograms of the first, second, fifth, and 10th cycles. Peaks are assignable, respectively, as  $Ox_1/Red_1$ ,  $Ox_2/Red_2$ , and  $Ox_3$ . Changes of the current of each peak in the potential sweep cycles are shown in Fig. 3. The current of the oxidation peak  $Ox_3$  resulting from the oxidation of Fe<sub>3</sub>C decreased quickly along with the increase in the potential sweep cycle number and disappeared after the fifth cycle. This result indicates that Fe<sub>3</sub>C oxidation is an irreversible reaction and that Fe<sub>3</sub>C was consumed during the first five cycles. On the other hand, the current of Red<sub>2</sub> (Fe<sub>3</sub>O<sub>4</sub>  $\rightarrow$  Fe(OH)<sub>2</sub>) increased rapidly to a maximum at cycle 2 or 3 and then decreased gradually with increasing sweep cycle number, indicating an increase in the content of Fe<sub>3</sub>O<sub>4</sub> in the reductive reaction shown in (2) after the first cycle. The current of both Red<sub>2</sub> and Ox<sub>2</sub> increased with increasing sweep



Fig. 3. Change of redox peak current in cyclic voltammetry.



Fig. 4. Galvanostatic charge–discharge curves of Fe<sub>3</sub>C. Charge and discharge current density were  $50 \text{ mAg}^{-1}$ .

cycle number. Therefore, reaction (2) is inferred to take place reversibly. In addition, the current of  $Ox_1/Red_1$  (redox reactions between Fe(OH)<sub>2</sub> and Fe) apparently increased at the second cycle and then leveled off. These results indicate that Fe<sub>3</sub>C was oxidized irreversibly into Fe<sub>3</sub>O<sub>4</sub> and that the Fe<sub>3</sub>O<sub>4</sub> produced by oxidation of Fe<sub>3</sub>C was reduced to Fe through Fe(OH)<sub>2</sub> in the cathodic sweep. It can therefore be concluded that the reversible redox reactions of Fe<sub>3</sub>O<sub>4</sub>  $\rightleftharpoons$  Fe(OH)<sub>2</sub>  $\rightleftharpoons$  Fe takes place after the oxidation of Fe<sub>3</sub>C to produce Fe<sub>3</sub>O<sub>4</sub>.

Fig. 4 shows discharge and charge curves of Fe<sub>3</sub>C in discharge-charge cycle measurements. In the curve of the first discharge, only one plateau, A, was observed at -0.85 V versus Ag/AgCl because of the oxidation of Fe<sub>3</sub>C to produce Fe<sub>3</sub>O<sub>4</sub>. At the second discharge, two plateaus, B and C, appeared, respectively, at ca. -1.05 and -0.9 V versus Ag/AgCl. Plateaus B and C are considered to stem, respectively, from the electrochemical oxidation of Fe to  $Fe(OH)_2$  (1) and  $Fe(OH)_2$  to  $Fe_3O_4$  (2). Because the rapid fall of potential occurs at the same value of plateau A, ca. -0.8 V versus Ag/AgCl, oxidation of Fe<sub>3</sub>C is likely to take place in parallel with oxidation of Fe(OH)<sub>2</sub> to  $Fe_3O_4$ . In the charge curve, plateau D was observed between -1.05 and -1.1 V versus Ag/AgCl. The charging plateau D corresponds to the reduction of Fe<sub>3</sub>O<sub>4</sub> produced through oxidation of Fe<sub>3</sub>C. During charging, hydrogen bubbles were generated by water electrolysis in the region of -1.1 to -1.2 V versus Ag/AgCl (E). In that region, the reduction of Fe(OH)<sub>2</sub> to Fe also occurs in parallel with hydrogen evolution, indicating the low coulomb efficiency of Fe(OH)<sub>2</sub> reduction.

Table 1 shows the composition of  $Fe_3C$  particles before discharge–charge cycle measurement and after six discharge– charge cycles, as determined by Mössbauer spectroscopy. It is apparent that the  $Fe_3C$  content decreased and  $Fe_3O_4$  content

Table 1

Composition of active material before and after charge-discharge cycle measurements

	Before (wt.%)	After (wt.%)
Fe <sub>3</sub> C	89.5	73.0
Fe <sub>3</sub> O <sub>4</sub>	10.5	19.7
Fe	0.0	7.3



Fig. 5. Dependence of discharge/charge capacity of Fe<sub>3</sub>C on the cycle number.



Fig. 6. SEM photographs of Fe $_3C$  particles before (a) and after (b) charge–discharge measurements.

increased after discharge–charge cycles. In addition, the increase of Fe content in the sample was observed after cycle measurements. The increase of  $Fe_3O_4$  content after discharge–charge cycles also suggests that  $Fe_3C$  is oxidized to  $Fe_3O_4$  during discharge. In addition, the appearance of Fe is considered to result from the reduction of  $Fe_3O_4$ . From the results of Mössbauer spectroscopy, it is uncertain how carbon behaves in discharge–charge cycles. Considering the electrochemical stability of carbon, it is likely to remain unchanged in the electrode.



Fig. 7. Reflection electron images of an electrode before (a) and after (b) charge–discharge measurements. The bright spots in the images indicate the existence of iron species.

Fig. 5 shows the relationship between the cycle number and discharge capacity. The discharge capacity of the second discharge was observed to be about 1.5 times greater than that of the first discharge and even greater than the charge capacity of the first charge. In discharges 3–5, coulomb efficiency is apparently more than 100%, as in the second discharge. These results suggest that the structural change of electrode particles occurred and the fresh Fe<sub>3</sub>C became exposed to electrolyte. After the second discharge, the capacity decreased quickly as the cycle number increased, implying the passivation of iron species.

Scanning electron microscopy (SEM) was performed to investigate the structural change of electrode particles. Some SEM images of samples before discharge-charge cycle measurement and after six discharge-charge cycles are shown in Fig. 6(a) and (b). Before discharge-charge cycle measurement, many pores with diameter of several 100 nm were observed on the surfaces of the 5-20 µm particles. In contrast, during charge-discharge cycles, the particles became more spherical than the original particles. Average diameters of electrode particles after six charge-discharge cycles were observed to be less than 100 nm. In addition, reflection electron images (Fig. 7(a) and (b)) indicate uniform dispersion of Fe<sub>3</sub>C particles on the surface of carbon black particles after six charge-discharge cycles. Hang et al. [9,10] observed a similar phenomenon in the case of the mixture of Fe or Fe<sub>2</sub>O<sub>3</sub> and carbon materials. They concluded that this phenomenon is attributable to the dissolution and deposition processes of Fe and Fe(OH)<sub>2</sub> via an intermediate species of iron:  $HFeO_2^{-}$  [2,11]. Our measurements show that the Fe<sub>3</sub>O<sub>4</sub> that is produced through oxidation of Fe<sub>3</sub>C is reduced to Fe through Fe(OH)<sub>2</sub>. Therefore, it is likely that the uniform dispersion of iron nanoparticles is attributable to the dissolution-deposition process between Fe and Fe(OH)<sub>2</sub> via  $HFeO_2^{-}$ . In addition, dissolution of these iron species seems to have caused the exposure of fresh Fe<sub>3</sub>C surfaces, thereby creating more discharge capacity than the charge capacity.

In conclusion, all processes of charge–discharge in an Fe<sub>3</sub>C electrode can be summarized as shown in Fig. 8. In the discharge process, Fe<sub>3</sub>C is oxidized irreversibly to Fe<sub>3</sub>O<sub>4</sub>. During charging, the produced Fe<sub>3</sub>O<sub>4</sub> is subsequently reduced to Fe(OH)<sub>2</sub> and Fe, contributing to the increased discharge



Fig. 8. Schematic diagram of the reaction of Fe<sub>3</sub>C in alkaline electrolyte.

capacity after the second discharge. In the redox reaction of  $Fe(OH)_2$  and Fe, they are likely to be dissolved and deposited through the intermediate ion of  $HFeO_2^-$ , thereby causing the uniform deposition of iron nanoparticles on the electrode surface.

# 4. Conclusions

Iron carbide ( $Fe_3C$ ) was applied as the active material of an anode of an alkaline battery and the charge-discharge reaction scheme of Fe<sub>3</sub>C was investigated. Results of cyclic voltammetry, galvanostatic discharge-charge measurement and Mössbauer spectroscopy indicated that Fe<sub>3</sub>C was oxidized irreversibly into Fe<sub>3</sub>O<sub>4</sub> during the discharge process and that the produced Fe<sub>3</sub>O<sub>4</sub> was reduced to Fe(OH)<sub>2</sub> or Fe during the charge process. Results also showed that Fe and Fe(OH)<sub>2</sub> produced during the charge process were oxidized electrochemically after subsequent discharge in parallel with the electrochemical oxidation of Fe<sub>3</sub>C. After discharge-charge cycles, Fe<sub>3</sub>C particles were observed to change their shape to spherical particles with less than 100nm diameter. It is likely that this result was caused by the dissolution-deposition process of Fe(OH)2 and Fe via intermediate iron species. The authors infer that fresh surfaces of Fe<sub>3</sub>C are exposed to alkaline electrolyte as a result of this dissolution-deposition process, exhibiting apparent coulomb efficiency of more than 100% in discharges 2-5.

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